

# IWA Wastewater

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## Optimization of the pilot-scale NPHarvest process in field tests using digester reject water

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inspiring change



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# N & P RECOVERY

- P is limited resource
- P natural resources are controlled by just few countries
  - Conflicts can have volatile effects on availability & prices
- N capture from air is energy intensive
- N removal in biological process is energy intensive and produces  $N_2O$
- -> we should recover both!



# GOAL OF THE STUDY AND TESTS IN VIKINMÄKI WWTP

- Understand process conditions' effects on performance in real conditions
- Ammonia transfer efficiency
- Hydraulic retention time (HRT)
- Acid strength and type
- Bulk liquid pH
- Tests were conducted with Viikinmäki WWTP digester reject water
- High SS, high  $\text{NH}_4$ , low P content

| Run No. | Run purpose   | HRT (h) | Acid type                     | Bulk pH |
|---------|---------------|---------|-------------------------------|---------|
| #1      | HRT           | 8       | 1M $\text{H}_2\text{SO}_4$    | 11      |
| #2      | HRT           | 4       | 1M $\text{H}_2\text{SO}_4$    | 11      |
| #3      | HRT           | 2       | 1M $\text{H}_2\text{SO}_4$    | 11      |
| #4      | Acid strength | 8       | 2M $\text{H}_2\text{SO}_4$    | 11      |
| #5      | Acid strength | 8       | 0.5M $\text{H}_2\text{SO}_4$  | 11      |
| #6      | Bulk pH       | 8       | 1M $\text{H}_2\text{SO}_4$    | 10      |
| #7      | Bulk pH       | 8       | 1M $\text{H}_2\text{SO}_4$    | 9       |
| #8      | Acid type     | 8       | 0.5 M $\text{H}_3\text{PO}_4$ | 11      |
| #9      | Acid type     | 8       | 0.5 M $\text{HNO}_3$          | 11      |





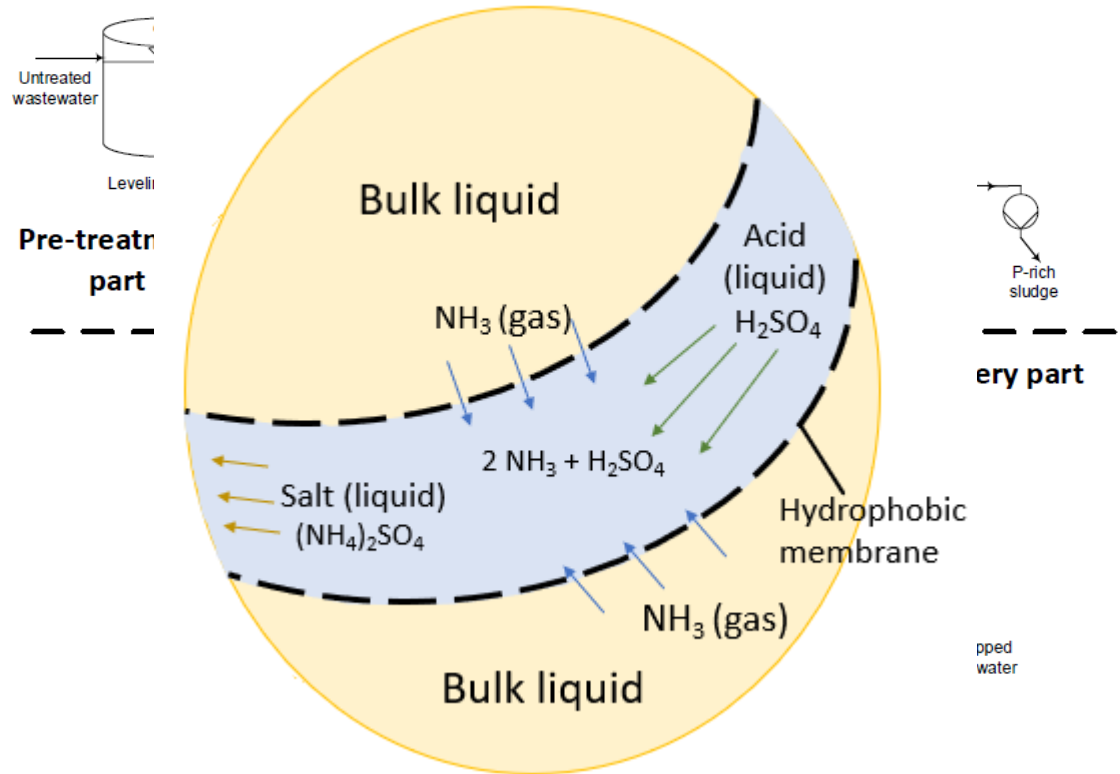
# NPHARVEST PROCESS



- Pre-treatment
- P recovery & SS removal
- P product: P, Ca and C
- N recovery
- Hydrophobic membranes
- N product: ammonia salt

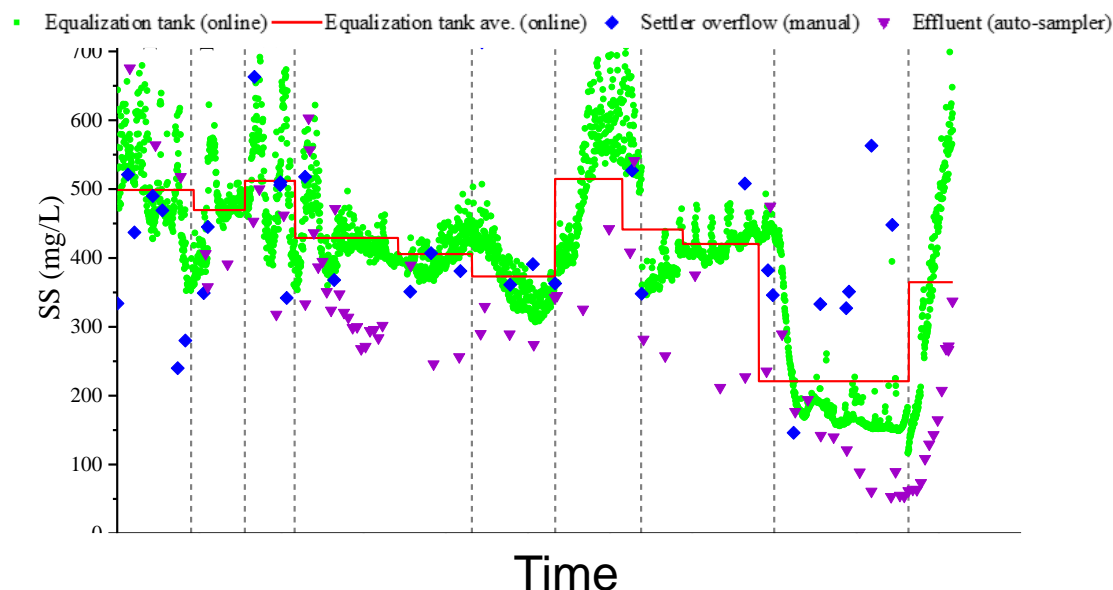
## Benefits:

- Low energy consumption
- Robust SS tolerance



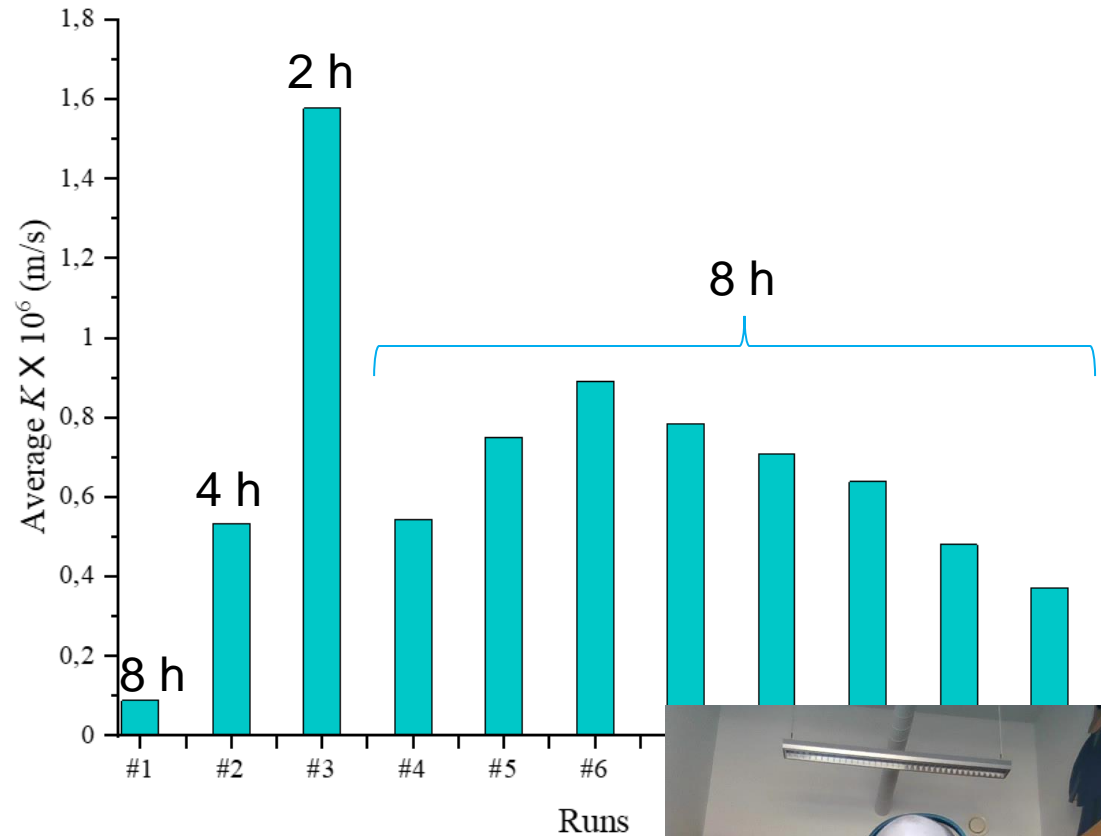
# SUSPENDED SOLIDS TOLERANCE

- Membrane contactor has robust SS tolerance
- ~500 mgSS/L does not interfere with ammonia recovery
- Lowest SS concentration was when organic polymer was used instead of PAX and polymer



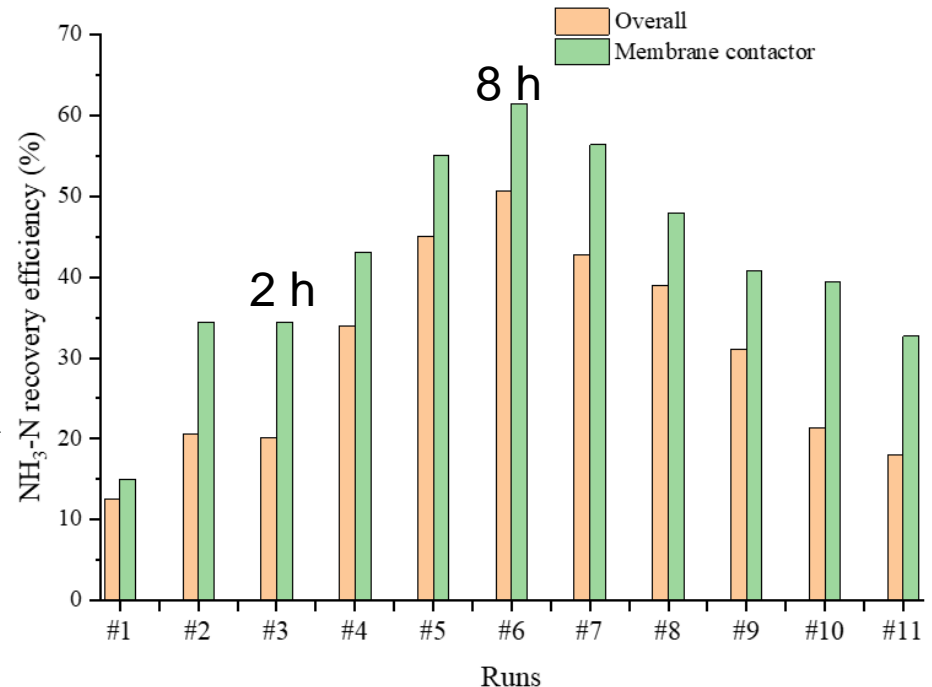
# HYDRAULIC RETENTION TIME

- Short HRT = high flow rate
- Shorter HRT demonstrated better ammonia transfer rate
- Higher flow rate decreases ammonia concentration polarization
- -> promotes ammonia mass transfer rate



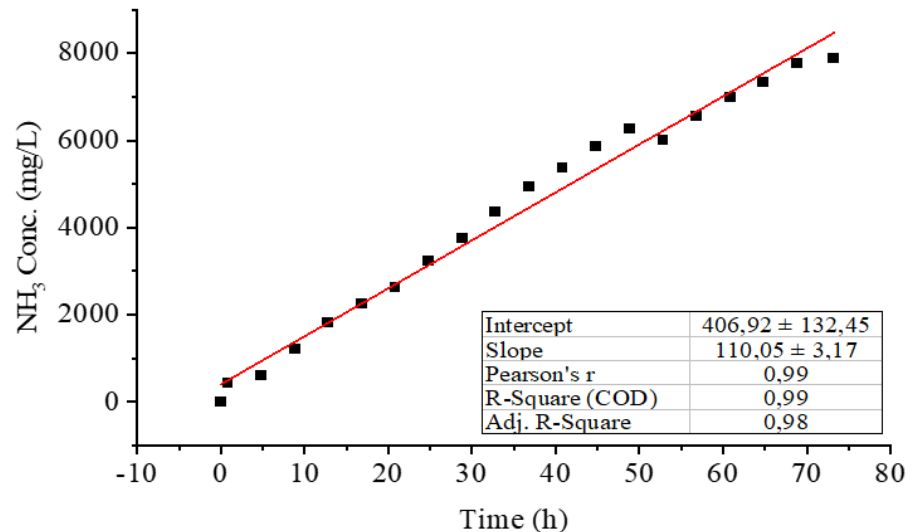
# HRT & RECOVERY EFFICIENCY

- Note! High transfer rate does not automatically mean high recovery efficiency
- Longer HRT promotes recovery efficiency
- -> Overall process design is a balance between recovery efficiency and transfer rate
- Also note: goal of the study was not to maximize recovery efficiency



# BULK LIQUID PH

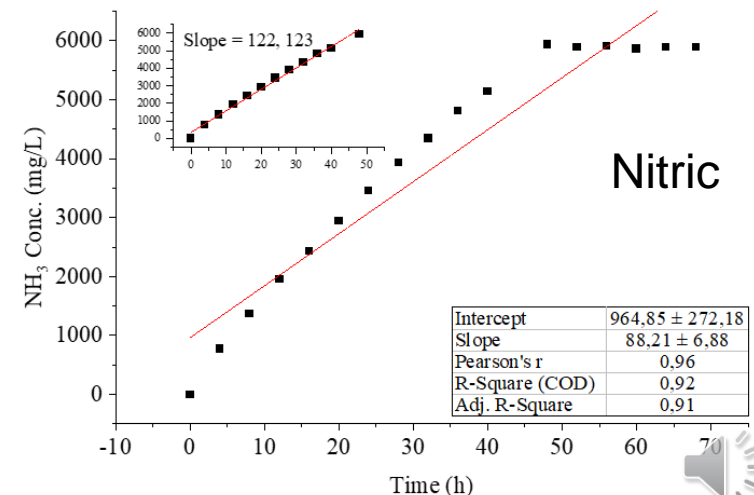
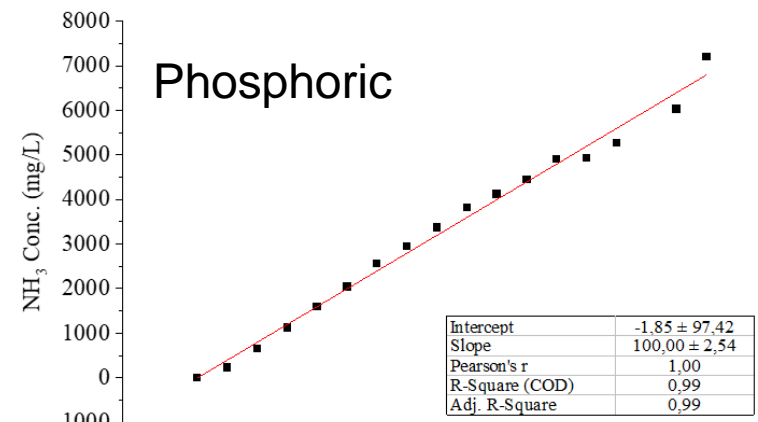
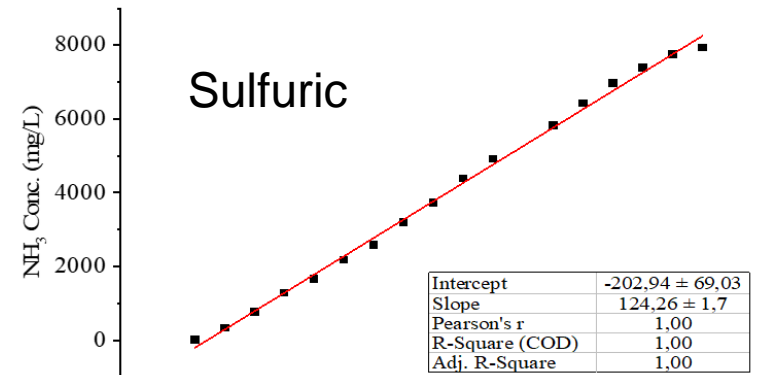
- Ammonia balance shifts towards  $\text{NH}_3$  when pH increases
  - The slope of ammonia concentration shows transfer efficiency
  - pH 9 slope: 87
  - pH 10 slope: 110
  - pH 11 slope: 51
- 
- pH 10 is the most efficient in terms of ammonia transfer (and chemical consumption!)





# AMMONIA STRIPPING ACID

- 0.5 mol/L showed highest transfer rate
- Sulfuric acid and nitric acid had similar transfer rate
- Phosphoric acid was slightly lower
- Acid choice is further affected by desired end product



# CONCLUSIONS

- Tests in real environment were conducted to understand the process conditions' effect on ammonia transfer rate
- The best conditions for ammonia recovery are:
- Low HRT while maintaining good recovery efficiency
- Bulk liquid pH 10
- 0.5 mol/L acid concentration
- Nitric and sulfuric acid had better transfer rate



# THANK YOU!

- For you interest!



**KEEP  
CALM  
AND  
ASK  
QUESTIONS**

